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air movement in buildings

Computerprograms calculating air pressures and air flows in buildings in which a fire is simulated

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Report C 411 February 1978

Sound, light and indoor climate division

Project nr. 1.3.16 (20030138)



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C 411

February 1978

IG-TNO/Dep. GLB

JP/JN

SUMMARY

Three computerprograms calculating air pressures and air flows in buildings have been developed.

These computer programs consist of a network of non-linear equations. The IWIS libraryprocedure KNEWTØN is used in the iteration process which finds the solution of the system of nonlinear equations. Rooms in which several air flows come together are called junctions (for instance a corridor, a central hall or a staircase).

The first program is suited for a model with one junction, the second one for a model with one junction and a room in which a fire can be simulated. With the third program it is possible to calculate flows and pressures in a model with one fireroom and nineteen junctions.

1. INTRODUCTION

In order to deal with the smokeproblem in buildings in case of fire, one has to get a better understanding of the importance of the different factors determining the spread of smoke through the building.

These factors are:

1. the windpressure around the building
2. the air leakage of the facade and inner walls
(i.e. windows, doors and other openings)
3. the temperature differences (i.e. caused by the fire)
4. mechanical ventilation
5. smokeproduction

These factors can serve as input data for a computerprogram as air flows, air pressures, pressuredifferences and air leakage coefficients (C-values).

In the ventilation technique it is common use to approximate the air flow through a gap or a crack with the equation:

$$I_m = C_m \cdot (\Delta p)^{1/n} \quad (1)$$

where I_m = air mass flow [kg.s⁻¹]
 C_m = air mass leakage [kg.s⁻¹] at 1 [Pa]
 Δp = pressure difference across the gap [Pa]
 n = exponent between 1 and 2
 laminar flow, $n = 1$
 turbulent flow, $n = 2$

The model of a building can be very extensive and complex. Often one is not interested in each individual flow and pressure. In that case it may be useful to simplify the model. This is possible by calculating the substitute for serial and parallel branches.

The smoke problem is a dynamic one.

By calculating the proposed model at several thermal pressure differences one can obtain a sufficient approximation of the dynamic process. Because of the breaking of window panes during the fire the C-values will have a very discontinuous course.

2. CONCLUSION

These computer programs are a very useful tool to obtain information about a large scope of proposed systems or situations of buildings in which a fire may cause spread of smoke. Though buildings can be more complex than indicated in these programs, we think that the most important influences on the spread of smoke can be calculated if the right simplifications are made.

3. THE COMPUTERPROGRAMS

3.1 Computer language

The programs have been written in FORTRAN 4 for the CDC 6000 computer. In order to use the computerprogram the following group of cards has to be inserted in the card reader:

Example: First program.

JOBNAME, T40, I040, CM 52000. ---. + your name
ACC0UNT, ----- + your computer account number
REWIND, 0UTPUT.

FTN.

LG0

7/8/9

+ end of record

PROGRAM JA (INPUT, OUTPUT)

COMMON // Y, C(10,3)

.

.

} the text of
this program

7/8/9

+ e.o.r.

.

.

.

} input data

6/7/8/9

+ end of

Second and third program

JOBNAME, T ..., I0..., CM....

Name

ACC0UNT,

REWIND, 0UTPUT

ATTACH, FILE, ACCULIB, ID = PSL, MR = 1

LIBRARY, FILE

FTN

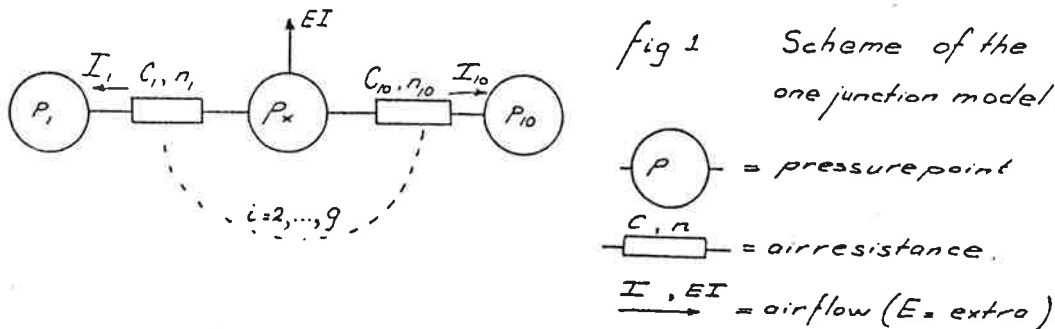
LG0

7/8/9

and further identical to the first program.

3.2.1 One Junction

The first problem was



A model with one junction with an unknown pressure p_x and a maximum of ten flows coming together in the junction. As mentioned in the introduction one flow can be represented by a simple equation.

$$I_i = C_i * (p_x - p_i)^{1/n_i}, \quad i = 1, \dots, 10 \dots \quad (2)$$

The pressure p_x can be calculated by the equation

$$\sum_{i=1}^{10} C_i * (p_x - p_i)^{1/n_i} + EI = 0 \quad (3)$$

This equation is nonlinear in the pressure p_x and p_i .
 EI is a flow caused by the mechanical ventilation.

If $p_x - p_i$ is negative we must write (2):

$$\sum_{i=1}^{10} \text{sign}(p_x - p_i) * C_i * (\text{abs}(p_x - p_i))^{1/n_i} + EI = 0 \quad (4)$$

The only unknown variable is p_x

A short computerprogram finds the solution of this equation with a given tolerance EPS.

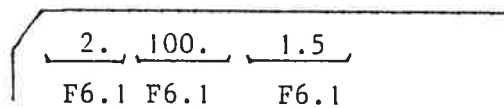
The iteration process in the program is based upon the bisection method.

N = 3
AO = -100.0
BO = 100.0
EPS = 0.0001
EI = 10.0

The next N cards, in this example the next 3, are read by the statement:

```
READ 102,( C (K,L), L = 1,3), K = 1,N)  
102 FØRMAT (3 F6.1)
```

Each card must be prepared in this way:



For example:

C (1,1) = 2.0
C (1,2) = 100.0
C (1,3) = 1.5

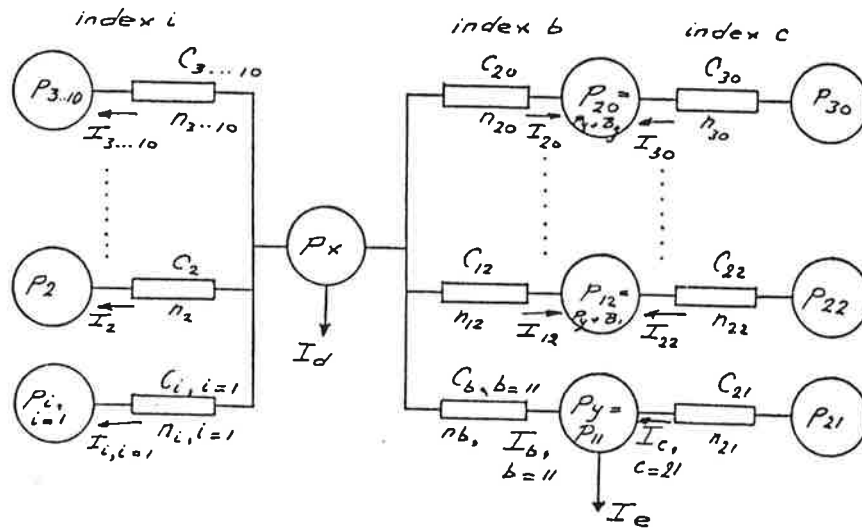
3.2.4 Output

The output values are:

- the pressure in the junction p_x
- the values of the flows around the junction.

3.3.1 Two Junctions

The second problem was



Two junctions with unknown pressures p_x and p_y and three groups of flows:

$$\begin{aligned} I_i & \quad i = 1, \dots, 10 \\ I_b & \quad b = 11, \dots, 20 \\ I_c & \quad c = 21, \dots, 30 \end{aligned}$$

where:

$$I_i = C_i * (p_x - p_i)^{1/n_i} ; i = 1, \dots, 10 \tag{5}$$

$$I_b = C_b * (p_x - p_b)^{1/n_b} ; b = 11, \dots, 20 \text{ and } p_{11} = p_y \tag{6}$$

$$I_c = C_c * (p_c - p_b)^{1/n_c} ; c = 21, \dots, 30 \tag{7}$$

$$p_{11} = p_y + B_0 \text{ where } B_0 = 0$$

$$p_{12} = p_y + B_1$$

⋮

$$p_{20} = p_y + B_9$$

(8)

$C_i, C_b, C_c, p_i, p_c, n_i, n_b, n_c$ and the differences between p_{11} and p_{12}, \dots, p_{20} (B_0, \dots, B_9) are known.

For this problem two nonlinear equations are valid:

$$\left. \begin{aligned} \sum_i I_i + \sum_b I_b + EI(1) &= 0 \\ \sum_b I_b + \sum_c I_c + EI(2) &= 0 \end{aligned} \right\} \dots (9)$$

In pressure, C-values and exponents:

$$\begin{aligned} \sum_{i=1}^N \text{sign}(p_x - p_i) * C_i * (\text{abs}(p_x - p_i))^{1/n_i} &+ \sum_{b=11}^{10+K} \text{sign}(p_x - p_y - B_{b-11}) * C_b * \\ &(\text{abs}(p_x - p_y - B_{b-11}))^{1/n_b} + EI(1) = 0 \\ \sum_{b=11}^{10+K} \text{sign}(p_x - p_y - B_{b-11}) * C_b * (\text{abs}(p_x - p_y - B_{b-11}))^{1/n_b} &+ \sum_{c=21}^{20+M} \text{sign}(p_c - p_y - B_{c-21}) * C_c * \\ &(\text{abs}(p_c - p_y - B_{c-21}))^{1/n_c} - EI(2) = 0 \end{aligned} \quad (10)$$

Again, the only unknown variables are p_x and p_y .

The program uses the library procedure KNEWTØN of IWIS-TNO for the iteration process. This procedure computes the solution of this system of two nonlinear equations with two unknown variables by the method secant.

The procedure KNEWTØN calls the other procedures:

- F (2,X,Y) which calculates the left hand side of both equations.
The first value of them is placed in Y(1) and the second in Y(2)
- CHECK (2,X,Y,K) which uses the results in array X and Y and stops the iteration process when the solution has been sufficiently approximated.

3.3.2 Input data

N the number of flows I_i
 K " " " " I_b
 M " " " " I_c

EPS-the tolerance

EI (1)-the extra flow to the first junction

EI (2)-the extra flow to the second junction

C(i,1) i = 1,..., N The values of C, p and n
l = 1,2,3 (equation 1) at I_i

B(i,1) i = 1,..., K The values of C, B and n at I_n
l = 1,2,3

A(i,1) i = 1,..., M The values of C, p and n at I_c
l = 1,2,3

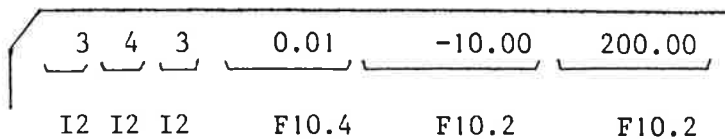
3.3.3 Preparing of input data

The first six input data are read by the statements

```
READ 1000, N, K, M, EPS, EI(1), EI(2)
```

```
1000 FØRMAT (3I2, F10.4, 2F10.2)
```

Example.



After this:

N = 3, K = 4, M = 3, EPS = 0.01, EI (1) = -10.0, EI (2) = 200.0

The next N, K and M cards are read by:

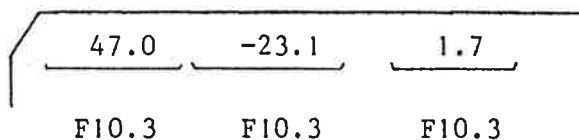
```
READ 1002, (( C(I,L), L = 1,3), I = 1,N)
```

```
READ 1002, (( B(I,L), L = 1,3), I = 1,K)
```

```
READ 1002, (( A(I,L), L = 1,3), I = 1,M)
```

```
1002 FØRMAT, (3 F10.3)
```

Example of one card, say the fifth card of the first group:



After this: C (5,1) = C₅ = 47 [kg.s⁻¹] at 1[Pa]

C (5,2) = p₅ = -23.1 [Pa]

C (5,3) = n₅ = 1.7

3.3.4 Output

The output values are:

p_x and p_y

Flow I_1, \dots, N .

Flow B_1, \dots, K .

Flow C_1, \dots, M .

3.4.1 Two and more junctions

The third problem to study was:

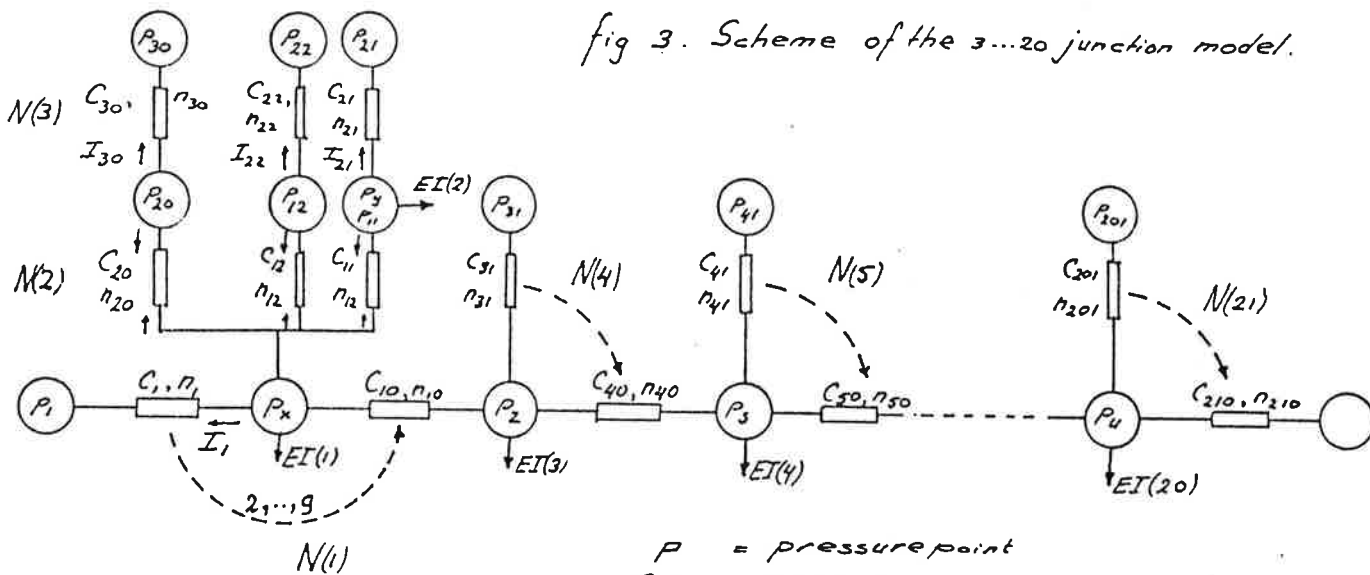


fig 3. Scheme of the 3...20 junction model.

p = pressure point
 C, n = air resistance
 I, EI = air flow (E = extra)
 N = group of flows of one junction.

There are NN junctions, $2 \leq NN \leq 20$, with NN unknown pressures $p_x, p_y, p_z, \dots, p_u$ and $(NN+1)$ flow groups $\Sigma I_1, \Sigma I_2, \dots, \Sigma I(NN), \Sigma I(NN+1)$.

These flow groups are described by NN nonlinear equations:

$$\begin{aligned}
 & N(1) \quad \sum_{i=1}^{N(1)} I1_i + \sum_{i=1}^{N(2)} I2_i + EI(1) = 0 \\
 & N(2) \quad \sum_{i=1}^{N(2)} -I2_i + \sum_{i=1}^{N(3)} I3_i + EI(2) = 0 \\
 & N(4) \quad \sum_{i=1}^{N(4)} I4_i + EI(3) - I1_{N(1)} = 0 \\
 & N(5) \quad \sum_{i=1}^{N(5)} I5_i + EI(4) - I4_{N(4)} = 0 \\
 & \cdot \\
 & \cdot \\
 & \cdot \\
 & N(NN) \quad \sum_{i=1}^{N(NN)} I(NN)_i + EI(NN-1) - I(NN-1)_{N(NN-1)} = 0 \\
 & N(NN+1) \quad \sum_{i=1}^{N(NN+1)} I(NN+1)_i + EI(NN) - I(NN)_{N(NN)} = 0
 \end{aligned} \tag{11}$$

where:

$$\begin{aligned}
 I1_i &= C_i * (p_x - p_i)^{1/n_i} & i = 1, \dots, 10 \\
 I2_i &= C_i * (p_x - B_{i-11} - p_y)^{1/n_i} & i = 11, \dots, 20 \\
 I3_i &= C_i * (p_y + B_{i-22} - p_y)^{1/n_i} & i = 21, \dots, 30 \\
 I4_i &= C_i * (p_z - p_i)^{1/n_i} & i = 31, \dots, 40 \\
 I5_i &= C_i * (p_s - p_i)^{1/n_i} & i = 41, \dots, 50 \\
 & \cdot \\
 & \cdot \\
 & \cdot \\
 I21_i &= C_i * (p_u - p_i)^{1/n_i} & i = 201, \dots, 210
 \end{aligned}$$

Exactly:

(Note: The notation of the pressure differences should be like in equation (4) and (10)).

$$\sum_{i=1}^{N(1)-1} C_i * (p_x - p_i)^{1/n_i} + C_{N(1)} * (p_x - p_z)^{1/n_{N(1)}} +$$

$$\sum_{i=1}^{N(2)} C_i * (p_x - B_{i-11} - p_y)^{1/n_i} + EI(1) = 0$$

$$\sum_{i=1}^{N(2)} C_i * (B_{i-11} - p_y - p_x)^{1/n_i} + \sum_{i=1}^{N(3)} C_i * (B_{i-11} + p_y - p_i)^{1/n_i} + EI(2) = 0$$

$$\sum_{i=1}^{N(4)-1} C_i * (p_z - p_i)^{1/n_i} + C_{N(4)} * (p_z - p_s)^{1/n_{N(4)}} + C_{N(1)} * (p_z - p_x)^{1/n_{N(1)}} +$$

$$+ EI(3) = 0 \dots(12)$$

$$\sum_{i=1}^{N(NN+1)} C_i * (p_u - p_i)^{1/n_i} + C_{N(NN)} * (p_u - p_w)^{1/n_{N(NN)}} + EI(NN) = 0$$

The computerprogram solves this system with the aid of some subroutines.

The job consists of:

- main program ELA
- subroutine F
- subroutine CHECK.

In the mainprogram input data are read and X1(NN) is given the value of the maximum of the known pressures and X2(NN) the minimum of them. X1(NN) and X2(NN) act as start vectors of the solution. They contain the pressures $p_x, p_y, p_z, \dots, p_u$. In the main program the maximum number of iterations is set to 500 and KNEWTØN is called, in which KNEW does the iteration process after CHECK has been called.

In CHECK and KNEW F is used. F calculates the left hand side of the equations (12) in the points X1 (NN) and X2 and puts those values to Y1(NN) and Y2 (NN). CHECK stops the iteration process if all absolute values of $|Y1(i)|_{i=1, \dots, NN}$ or those of $|Y2(i)|_{i=1, \dots, NN}$ are less than EPS. If not the program is set to KNEW for a new iteration step. Further more KNEWTØN uses DECOMP and SOLVE for matrix operations.

3.4.2. Input data

- NN - number of junctions + 1
- EPS - tolerance of the solution
- N(NN) - the number of flows around each junction
- EI(NN-1) - the extra flows (mech. ventilation or smoke production)
- A(NN,10,3) - the values of C, p and n for all flows.

These data are read by

```
      READ 1001, NN, EPS
1001  FØRMAT (I3, F10.4)
      READ 1002, (N(I), I + 1, NN)
1002  FØRMAT (2I13)
      READ 1006, (EI(J), J + 1, NN)
1006  FØRMAT (8F 10.3)
      READ 1003, (A(I, J, KM), KM + 1, 3), J = 1, NA) for I = 1, NN
1003  FØRMAT (3 F10.3)
```

Note that array A(I, J, K) contains all known C-values, pressures or pressure differences and exponents.

I is the number of the flowgroup (fig. 3).

J is the number of the flow in the flow group.

K = 1,3 (1 = C-value; 2 = pressure and 3 = exponent).

At the place of an unknown pressure (usually on the last card of a group of flows) can be any value, for it will not be read.

Those values for the unknown pressures are generated in the iteration subroutines of the program. In the second group of flows the pressure differences between the first pressure-point of the second group and the concerning pressure-point are written at the second place (K = 2) on the card.

3.4.3. Example of input data

card 1 : 7 0.01
 variable : I3 NN EPS

card 2 : 4 4 3 4 4 4 4
 variable : I3 I3 I3 I3 I3 I3 I3
 N(1) N(2) N(3) N(4) N(5) N(6) N(7) = N(NN)

card 3 : 100.0 -500.0 125.0 25.0 125.0
 F10.3 F10.3 F10.3 F10.3 F10.3
 variable : EI(1) EI(2) EI(3) EI(4) EI(5)
 8 times F10.3

All next cards are written in FØRMAT (3 F10.3)

variable :	C-value	pressure	exponent	
card 4 :	1.0	50.0	1.5	A (1,J,K) I = 1 2)
card 5 :	1.5	-20.0	1.7	
:	1.2	-30.0	1.7	1)
:	1000.0	<u>0.0</u>	2.0	
:	1000.0	0.0	2.0	A (2,J,K) I = 2
:	1000.0	2.0	2.0	
:	1000.0	5.0	2.0	
:	0.0	8.0	2.0	
:	500.0	-10.0	2.0	A (3,J,K) I = 3
:	500.0	-10.0	2.0	
:	500.0	-10.0	2.0	
:	1.5	70.0	1.5	A (4,J,K) ,,
:	2.0	-25.0	1.7	
:	1.0	-25.0	1.6	
:	1000.0	<u>0.0</u>	2.0	
:	200.0	75.0	2.0	A (5,J,K)
:	1.5	-30.0	1.5	
:	1.7	-35.0	1.5	
:	1000.0	<u>0.0</u>	2.0	A (6,J.K)
:	1.3	75.0	1.5	
:	1.5	-30.0	1.8	
:	1.7	-30.0	1.6	
:	1000.0	<u>0.0</u>	2.0	A (7,J,K)
:	1.2	80.0	1.5	
:	200.0	-35.0	2.0	
:	1.5	-40.	1.5	1) <u>0.0</u> unknown pressures, data is not necessary.
:	50.0	-50.0	1.8	

2) J and K are described in

3.4.4. Output

The sequence of the output is:

- 1) estimates of the start values of the unknown pressures
- 2) calculated pressures
- 3) calculated flows.

For further details see appendix program 3.

3.5.1. Final

More information about the operation of the CDC system

(about using any program) can be found in the book: SCØPE [1].

Complete information about the language Fortran 4 is given

in the book : FØRTRAN REFERENCE MANUAL [2] . Both books are at

the IWIS terminal.

4. NOMENCLATURE

A	= array
B	= thermal pressure difference [Pa]
AO, BO	= pressure interval
C	= C-value = air leakage coefficient [kg.s ⁻¹] at 1 [Pa]
EI	= extra flow (mechanical ventilation/smokegasgeneration)
EPS	= tolerance in the solution
I	= mass flow of air [kg/s]
I,J,K,M,N	= index
N,NN	= maximum value of an index
n	= exponent (see (1))
p	= pressure [Pa]

5. REFERENCES

- [1] SCOPE REFERENCE MANUAL. Models 72, 73, 74 version 3.4
6000 version 3.4. Corporate Headquarters 8100 34th Ave.
SO. Minneapolis, Minn. 55440.
- [2] FORTRAN VERSION 4 REFERENCE MANUAL. Revised vision 8100
34th Ave. SO. Minneapolis, Minn. 55440.

PROGRAM JA

73/72 OPT=1

FTN 4.6+433

```

1      PROGRAM JA(INPUT,OUTPUT)
      COMMON/CO(10,3),J,EI
      DIMENSION A(500),B(500)
      READ 100,J,A0,B0,EPS,EI
5      READ 102,((C(K,L),L=1,3),K=1,J)
      PRINT 104
      PRINT 106,((C(K,L),L=1,3),K=1,J)
      I=1
      A(I)=A0
10     B(I)=B0
      F1=FUN(A(I))
      F2=FUN(B(I))
      IF(F1#F2.GT.0) GOTO 50
15     F=FUN((A(I)+B(I))/2)
      PRINT 108,1,A(I),B(I),F
      IF(ABS(F).LE.EPS)GOTO 30
      IF(F.GT.0) GOTO 10
      A(I+1)=(A(I)+B(I))/2
      B(I+1)=B(I)
20     GOTO 20
10    A(I+1)=A(I)
      B(I+1)=(A(I)+B(I))/2
20    I=I+1
      GOTO 5
25    30 PAR=(A(I)+B(I))/2
      PRINT 110,PAR
      DO 40 L=1,J
      F=C(L,1)*(ABS(PAR-C(L,2)))**(1/C(L,3))
30     IF(PAR.LT.C(L,2)) F=-F
      PRINT 112,L,F
40    CONTINUE
      GOTO 60
50    CONTINUE
      PRINT 114,A0,B0
35    60 CONTINUE
100   FORMAT(12,2F5.1,F6.4,F10.2)
102   FORMAT(3F6.1)
104   FORMAT(* CONTROL DATA *)
106   FORMAT(1H ,3F5.1)
40    108 FORMAT(1H ,15,3F10.4)
110   FORMAT(* VALUE OF PRESSURE IS= *,F10.4)
112   FORMAT(2H 1,12,2H =,F10.4)
114   FORMAT(* OAD INITIAL PARAMETERS A0=*,F6.1,* B0=*,F6.1)
45    STOP
      END

```

FUNCTION FUN

73/72 OPT=1

FTN 4.6+433

```

REAL FUNCTION FUN(PAR)
COMMON//C(10,3),J,EI
F=0.0
K=1
DO 10 L=1,J
IF (PAR.LT.C(L,2)) K=-1
F=F+K*C(L,1)*(ABS(PAR-C(L,2)))** (1/C(L,3))
10 K=1
FUN=F+EI
RETURN
END

```

CONTROL DATA

2.0	100.0	1.5		
1.0	-80.0	1.7		
4.0	-100.0	2.0		
1	-100.0000	100.0000	10.0776	
2	-100.0000	0.0000	-20.7836	
3	-50.0000	0.0000	-4.7971	
4	-25.0000	0.0000	2.7222	
5	-25.0000	-12.5000	-1.0114	
6	-18.7500	-12.5000	.8612	
7	-18.7500	-15.6250	-.0736	

VALUE OF PRESSURE IS= -17.1875

I 1 = -47.8943

I 2 = 11.4202

I 3 = 36.4005

PROGRAM ELA

73/72 OPT=1

FTN 4.6+433

```

PROGRAM ELA(INPUT,OUTPUT)
COMMON//J,C(10,3),K,B(10,3),M,A(10,3),EI(2),EPS
COMMON/NUM/LICZ
INTEGER R
REAL MIN,MAX,EI(2),X1(2),X2(2)
EXTERNAL KNEWTON,KNEW,DECOMP,SOLVE,F,CHECK
NN=2
N=500
LICZ=0
READ 1000,J,K,M,EPS,(EI(R),R=1,2)
READ 1002,((C(I,L),L=1,3),I=1,J)
READ 1002,((B(I,L),L=1,3),I=1,K)
READ 1002,((A(I,L),L=1,3),I=1,M)
PRINT 1001,J,K,M,EPS,(EI(R),R=1,2)
PRINT 1004,((C(I,L),L=1,3),I=1,J)
PRINT 1004,((B(I,L),L=1,3),I=1,K)
PRINT 1004,((A(I,L),L=1,3),I=1,M)

```

```

C
C-----MIN I MAX OF PRESSURE
C

```

```

MIN=MAX=0.0
DO 10 I=1,J
IF(C(I,2).LT.MIN)MIN=C(I,2)
IF(C(I,2).GT.MAX)MAX=C(I,2)
10 CONTINUE
DO 20 I=1,M
IF(A(I,2).LT.MIN)MIN=A(I,2)
IF(A(I,2).GT.MAX)MAX=A(I,2)
20 CONTINUE
X1(1)=2*MIN
X1(2)=2*MAX
X2(1)=MIN
X2(2)=MAX
PRINT 1005,(X1(KK),KK=1,2)
PRINT 1006,(X2(KK),KK=1,2)
CALL KNEWTON(NN,X1,X2,F,CHECK,N)
1000 FORMAT(3I2,F10.4,2F10.2)
1002 FORMAT(3F10.3)
1001 FORMAT(1H ,3I2,F10.4,2F10.2)
1004 FORMAT(1H ,3F10.3)
1005 FORMAT(* FIRST ESTIMATIONS OF SOLUTION IS *,2F10.3)
1006 FORMAT(* SECOND ESTIMATIONS OF SOLUTION IS *,2F10.3)
STOP
END

```

SUBROUTINE F

73/72 OPT=1

FTN 4.6+433

```

SUBROUTINE F(K1,X1,X2)
COMMON//J,C(10,3),K,B(10,3),M,A(10,3),EI(2),EPS
INTEGER R
REAL EI(2)
REAL X1(2),X2(2)
FU=0,
N=1

```

```

DO 10 I=1,J
  N=1
  IF((X1(1)-C(I,2)).LT.0)N=-1
10 FU=FU+N*C(I,1)*(ABS(X1(1)-C(I,2)))**(1/C(I,3))
  GU=0.
  DO 20 I=1,K
    N=1
    IF((X1(1)-X1(2)-B(I,2)).LT.0)N=-1
    GU=GU+N*B(I,1)*(ABS(X1(1)-X1(2)-B(I,2)))**(1/B(I,3))
20 FU=FU+N*B(I,1)*(ABS(X1(1)-X1(2)-B(I,2)))**(1/B(I,3))
  X2(1)=FU+CI(2)
  DO 30 I=1,M
    N=1
    IF((X1(2)+B(I,2)-A(I,2)).GT.0)N=-1
30 GU=GU+N*A(I,1)*(ABS(X1(2)+B(I,2)-A(I,2)))**(1/A(I,3))
  X2(2)=GU+CI(1)
  RETURN
  END

```

SUBROUTINE CHECK 73/72 OPT=1

FTN 4.6+433

```

SUBROUTINE CHECK(N1,X1,X2,K1)
COMMON/J,C(10,3),K,B(10,3),M,A(10,3),EI(2),EPS
COMMON/NUM/LICZ
INTEGER R
REAL X1(2),X2(2),Y1(2),Y2(2)
LICZ=LICZ+1
CALL F(2,X1,Y1)
CALL F(2,X2,Y2)
IF(ABS(Y1(1)).LT.EPS.AND.ABS(Y1(2)).LT.EPS)GOTO 50
PRINT 2,(X1(KK),KK=1,2),(Y1(KK),KK=1,2)
2 FORMAT(* VARIABLES *,2F20.10,* VALUES *,2F20.10)
IF(ABS(Y2(1)).LT.EPS.AND.ABS(Y2(2)).LT.EPS)GOTO 60
PRINT 2,(X2(KK),KK=1,2),(Y2(KK),KK=1,2)
RETURN
50 CONTINUE
PRINT 1,(X1(J),J=1,2)
X=X1(1)
Y=X1(2)
1 FORMAT(* VALUE OF PRESSURE IS X=... ; Y=... ; *,2F20.10)

GOTO 70
60 X=X2(1)
Y=X2(2)
PRINT 1,(X2(J),J=1,2)
70 DO 80 I=1,J
  N=1
  IF((X-C(I,2)).LT.0)N=-1
  FI=N*C(I,1)*(ABS(X-C(I,2)))**(1/C(I,3))
  PRINT 3,I,FI
80 CONTINUE
DO 90 I=1,K
  N=1
  IF((X-Y-B(I,2)).LT.0)N=-1
  FB=N*B(I,1)*(ABS(X-Y-B(I,2)))**(1/B(I,3))
  PRINT 4,I,FB
90 CONTINUE
DO 100 I=1,M
  N=1
  IF((Y+B(I,2)-A(I,2)).LT.0)N=-1
  FC=N*A(I,1)*(ABS(Y+B(I,2)-A(I,2)))**(1/A(I,3))
  PRINT 5,I,FC
100 CONTINUE

```

```

3 FORMAT(* FLOW I*,12,* = *,F20.10)
4 FORMAT(* FLOW H*,12,* = *,F20.10)
5 FORMAT(* FLOW C*,12,* = *,F20.10)
PRINT 6,LICZ
6 FORMAT(* NUMBER OF ITERATIONS IS *,I4)
K1=0
RETURN
END

```

```

6 4 4 .0100 0.00 0.00
2.100 2.160 1.500
1.100 -3.240 1.500
27.900 -3.240 1.700
2.700 -2.380 1.500
5.700 -2.380 1.800
1.500 -3.240 1.500
122.000 0.000 2.000
85.000 3.200 2.000
129.000 6.400 2.000
0.000 9.600 1.000
0.000 2.160 1.000
517.000 2.150 2.000
382.000 2.150 2.000
506.000 2.160 2.000

```

```

FIRST ESTIMATIONS OF SOLUTION IS -6.480 4.320
SECOND ESTIMATIONS OF SOLUTION IS -3.240 2.160

```

VALUE OF PRESSURE IS X=... ; Y=... ;

-1.1730652396 -4.2462557940

```

FLOW I 1 = -4.6857803253
FLOW I 2 = 1.7848856216
FLOW I 3 = 42.7651908376
FLOW I 4 = 3.0606903050
FLOW I 5 = 6.3278251967
FLOW I 6 = 2.4339349388
FLOW H 1 = 213.8722827467
FLOW H 2 = -30.2688651579
FLOW H 3 = -235.2901456175
FLOW H 4 = 0.0000000000
FLOW C 1 = 0.6000000000
FLOW C 2 = -925.7412732112
FLOW C 3 = -30.2137466393
FLOW C 4 = 904.2751143765

```

NUMBER OF ITERATIONS IS 9

FLA31,10100,1100,0452000.

WIL.

ACCOUNT,16,00000001,50.

REWIND,OUTPUT.

ATTACH,FILE,ACCULIB,TD=PSL,MR=1.

LIBRARY,FILE.

ETM.

LGO.

?

```

PROGRAM FLA(INPUT,OUTPUT)
COMMON//NN,N(21),A(21,10,3),EPS,EI(20)
COMMON/NUM/LIC7,K
REAL MIN,MAX
DIMENSION X1(20),X2(20)
EXTERNAL KNEWTON,KNEW,DECOMP,SOLVE,F,CHECK
READ 1001,NN,EPS
PRINT 1001,NN,EPS
IF (NN.GT.2.AND.NN.LT.22) GOTO 10
PRINT 1000
STOP

```

```

10 READ 1002,(N(I),I=1,NN)
PRINT 1002,(N(I),I=1,NN)
NNN=NN-1
READ 1006,(EI(J),J=1,NNN)
PRINT 1006,(EI(J),J=1,NNN)
DO 20 I=1,NN
NA=N(I)
READ 1003,((A(I,J,KM),KM=1,3),J=1,NA)
PRINT 1003,((A(I,J,KM),KM=1,3),J=1,NA)
20 CONTINUE

```

C
C.....MIN AND MAX OF PRESSURE
C

```

MIN=MAX=0.
DO 40 I=1,NN
IF (I.EQ.2) GOTO 40
NA=N(I)
DO 30 J=1,NA
IF (A(I,J,2).LT.MIN) MIN=A(I,J,2)
IF (A(I,J,2).GT.MAX) MAX=A(I,J,2)
30 CONTINUE
40 CONTINUE
DO 50 I=1,NNN
X1(I)=MAX
50 X2(I)=MIN
PRINT 1004,(X1(I),I=1,NNN)
PRINT 1005,(X2(I),I=1,NNN)
K=500
LIC7=0

```

C
C..... START TO ITERATIONS PROCESS
C

```

CALL KNEWTON(NNN,X1,X2,F,CHECK,K)
1000 FORMAT(* SORRY, YOU WANT TO SOLVE MORE THEN 20 OR LESS THEN 2
NONLINEAR EQUATIONS *)
1001 FORMAT(I3,F10.4)
1002 FORMAT(2I3)
1003 FORMAT(3F10.3)
1004 FORMAT(* FIRST ESTIMATIONS OF SOLUTION IS*,10F10.3,/,34X,10F10.3)
1005 FORMAT(* SECOND ESTIMATIONS OF SOLUTION IS*,10F10.3,/,34X,10F10.3)
1006 FORMAT(3F10.3)
STOP
END

```



```

SUBROUTINE F(LN,X1,X2)
COMMON/NN,N(21),A(21,10,3),EPS,EI(20)
DIMENSION X1(20),X2(20)
FU=0.
NA=N(1)
IF(NN.GT.7) NA=NA-1
DO 10 J=1,NA
M=1
IF((X1(1)-A(1,J,2)).LT.0)M=-1
10 FU=FU+M*A(1,J,1)*(ABS(X1(1)-A(1,J,2)))**(1/A(1,J,3))
IF(NN.EQ.3) GOTO 20
M=1
IF((X1(1)-X1(3)).LT.0)M=-1
FU=FU+M*A(1,N(1),1)*(ABS(X1(1)-X1(3)))**(1/A(1,N(1),3))
20 GU=0.
NA=N(2)
DO 30 J=1,NA
M=1
IF((X1(1)-X1(2)-A(2,J,2)).LT.0)M=-1
GU=GU+M*A(2,J,1)*(ABS(X1(1)-X1(2)-A(2,J,2)))**(1/A(2,J,3))
30 FU=FU+M*A(2,1,1)*(ABS(X1(1)-X1(2)-A(2,J,2)))**(1/A(2,J,3))
X2(1)=FU+EI(1)
NA=N(3)
DO 40 J=1,NA
M=1
IF((X1(2)+A(2,J,2)-A(3,J,2)).LT.0)M=-1
40 GU=GU+M*A(3,J,1)*(ABS(X1(2)+A(2,J,2)-A(3,J,2)))**(1/A(3,J,3))
X2(2)=GU+EI(2)
IF(LN.EQ.2) RETURN
DO 100 I=4,NN
NA=N(J)-1
M=1
IF(J.EQ.4)GOTO50
SR00=X1(J-1)-X1(J-2)
IF(SR00.LT.0)M=-1
FU=M*A(J-1,N(J-1),1)*ABS(SR00)**(1/A(J-1,N(J-1),3))
GOTO 60
50 SR00=X1(J)-X1(1)
IF(SR00.LT.0)M=-1
FU=M*A(1,N(1),1)*ABS(SR00)**(1/A(1,N(1),3))
60 DO 70 I=1,NA
M=1
SR00=X1(J-1)-A(J,I,2)
IF(SR00.LT.0)M=-1
70 FU=FU+M*A(J,I,1)*ABS(SR00)**(1/A(J,I,3))
IF(J.LT.NN)GOTO 80
M=1
SR00=X1(J-1)-A(J,N(J),2)
IF(SR00.LT.0)M=-1
FU=FU+M*A(J,N(J),1)*ABS(SR00)**(1/A(J,N(J),3))
X2(J-1)=FU+EI(J-1)
RETURN
80 M=1
SR00=X1(J-1)-X1(J)
IF(SR00.LT.0)M=-1
FU=FU+M*A(J,N(J),1)*ABS(SR00)**(1/A(J,N(J),3))
100 X2(J-1)=FU+EI(J-1)
RETURN
END

```

```

SUBROUTINE CHECK(LN,X1,Y2,K)
COMMON/NN,N(2),A(21,10,3),EPS,EI(20)
COMMON/NUM/LICZ,K1
DIMENSION X1(20),X2(20),Y1(20),Y2(20),X(20)
LICZ=LICZ+1
CALL F(LN,X1,Y1)
IF(LICZ.GT.50)GOTO 8
PRINT 2,(Y1(J),J=1,LM)
8 DO 10 J=1,LM
IF(ABS(Y1(J)).GT.EPS)GOTO 140
10 CONTINUE
DO 20 J=1,LM
20 X(J)=X1(J)
30 PRINT 1
PRINT 2,(X(J),J=1,LM)
NA=N(1)
MM=1
IF(NN.GT.3)NA=NA-1
DO 40 J=1,NA
M=1
SROD=X(1)-A(1,J,2)
IF(SROD.LT.0)M=-1
FU=M*A(1,J,1)*ABS(SROD)**(1/A(1,J,3))
PRINT 3,MM,J,FU
40 CONTINUE
IF(NN.EQ.3)GOTO 50
M=1
SROD=X(1)-Y(3)
IF(SROD.LT.0)M=-1
FU=M*A(1,N(1),1)*ABS(SROD)**(1/A(1,N(1),3))
PRINT 3,MM,N(1),FU
50 NA=N(2)
MM=2
DO 60 J=1,NA
M=1
SROD=X(1)-X(2)-A(2,J,2)
IF(SROD.LT.0)M=-1
FU=M*A(2,J,1)*ABS(SROD)**(1/A(2,J,3))
PRINT 3,MM,J,FU
60 CONTINUE
NA=N(3)
MM=3
DO 70 J=1,NA
M=1
SROD=X(2)+A(2,J,2)-A(3,J,2)
IF(SROD.LT.0)M=-1
FU=M*A(3,J,1)*ABS(SROD)**(1/A(3,J,3))
PRINT 3,MM,J,FU
70 CONTINUE
IF(NN.EQ.3)GOTO 130
JED=1
DO 120 J=4,NN
NA=N(J)-1
MM=J
M=1
DO 100 I=1,NA
M=1
SROD=Y(J-1)-A(1,I,2)
IF(SROD.LT.0)M=-1
FU=M*A(1,I,1)*ABS(SROD)**(1/A(1,I,3))
PRINT 3,MM,I,FU
100 CONTINUE

```

```

M=1
IF (J.LT.MN) GOTO 110
SR0D=X(J-1)-A(J,N(J),2)
IF (SR0D.LT.0) M=-1
FU=M*A(J,N(J),1)*ABS(SR0D)**(1/A(J,N(J),3))
PRINT 3,M,N(J),FU
GOTO 130
110 SR0D=X(J-1)-X(J)
IF (SR0D.LT.0) M=-1
FU=M*A(J,N(J),1)*ABS(SR0D)**(1/A(J,N(J),3))
PRINT 3,M,N(J),FU
120 CONTINUE
130 PRINT 4,LIC7
K=0
RETURN
140 CALL F(LN,X2,Y2)
IF (LIC7.GT.50) GOTO 145
PRINT 2,(Y2(J),J=1,LN)
145 DO 150 J=1,LN
IF (ABS(Y2(J)).GT.EPS) GOTO 140
X(J)=X2(J)
150 CONTINUE
GOTO 30
160 IF (LIC7.LT.K1) RETURN
PRINT 5
K=0
1 FORMAT(* VALUES OF PRESSURES *)
2 FORMAT(1H ,(5F20.10))
3 FORMAT(* FLOW I*,2I2,* = *,F20.10)
4 FORMAT(* NUMBER OF ITERATIONS IS *,I4)
5 FORMAT(* SORRY. THIS SYSTEM OF NONLINEAR EQUATIONS HAVE NO
RESOLUTION *)
RETURN
END

```

?

7	.01				
4	4	3	4	4	4
100.		-500.		125.	125.
1.		50.		1.5	140.
1.5		-20.		1.7	
1500.		-30.		2.	
1000.		0.		2.	
1000.		0.		2.	
1000.		2.		2.	
1000.		5.		2.	
0.		8.		2.	
500.		-10.		2.	
500.		-10.		2.	
500.		-10.		2.	
1.5		70.		1.5	
2.		-25.		1.7	
1.		-25.		1.6	
1000.		0.		2.	
200.		75.		2.	
1.5		-30.		1.5	
1.7		-35.		1.5	
1000.		0.		2.	
1.3		75.		1.5	
1.5		-30.		1.8	
1.7		-30.		1.6	
1000.		0.		2.	
1.2		80.		1.5	
200.		-35.		2.	
1.5		-40.		1.5	
50.		-50.		1.8	

?

VALUES OF PRESSURES

		<u>-19.7786259659</u>	<u>-19.4210373698</u>	<u>-19.5926700191</u>
		<u>-19.3070231693</u>	<u>-20.9068450562</u>	
		<u>-22.2413552230</u>		
FLOW	I 1 1 =		-16.9491537353	
FLOW	I 1 2 =		.6179339571	
FLOW	I 1 3 =		4795.6325757720	
FLOW	I 1 4 =		-431.2259810409	
FLOW	I 2 1 =		-597.9870366703	
FLOW	I 2 2 =		-1535.4440712790	
FLOW	I 2 3 =		-2314.6465164309	
FLOW	I 2 4 =		0.0000000000	
FLOW	I 3 1 =		-1534.6854213355	
FLOW	I 3 2 =		-1362.0790514723	
FLOW	I 3 3 =		-1051.3131514728	
FLOW	I 4 1 =		-30.0335206830	
FLOW	I 4 2 =		5.3975464890	
FLOW	I 4 3 =		2.8715362007	
FLOW	I 4 4 =		-534.4593996263	
FLOW	I 5 1 =		-1942.2360636060	
FLOW	I 5 2 =		7.2804296484	
FLOW	I 5 3 =		10.6557938620	
FLOW	I 5 4 =		1264.8406567440	
FLOW	I 6 1 =		-27.2380756735	
FLOW	I 6 2 =		5.1134083522	
FLOW	I 6 3 =		6.7553140047	
FLOW	I 6 4 =		1155.2100098111	
FLOW	I 7 1 =		-26.2380956561	
FLOW	I 7 2 =		714.3849040115	
FLOW	I 7 3 =		10.2101269835	
FLOW	I 7 4 =		316.8530749667	

NUMBER OF ITERATIONS IS 14

Simplified Flow diagram

