# ENERGY RECOVERY IN RECIRCULATION AIR SYSTEMS AND ITS CALCULATION OF DUST CONCENTRATION, RELATIVE HUMIDITY \& HEATER CAPACITY 

Song Ziyan ${ }^{1}$, Tan Kunxiong ${ }^{2}$, Chu Jiaming ${ }^{1}$<br>${ }^{1}$ TongJi University , Shanghai , China<br>${ }^{2}$ Hongkong Polytechnic University, Kowloon, Hongkong

## ABSTRACT

In some ventilation and dust removing system of workshop, a great deal of energy is wasted due to heated and cooled indoor air being exhausted directly. So if the dust in the indoor air is removed and then recirculate, the objective of energy saving can be reached. In this paper, the calculation equation of dust concentration, relative humidity in indoor and recirculate air and heater capacity are given along with the control measures to them. This kind of system has been practiced at a plant building located in heating region of northern China, the expectable result of energy saving was obtained, thus verified the conclusion in this paper.

## CONSTANT RECIRCULATE AIR VOLUME VENTLLATION AND DUST REMOVING SYSTEM

This kind of system is shown in Fig.1. Most of dust emitted during the process of production is collected by capturing hood then be delivered into dust separator along with air volume $V_{A}$. The cleaned $u p V_{P}$ then is returned into workshop. The dust concentration $C_{P}$ of $V_{P}$ depends on dust emission rate $\varepsilon$ the collection efficiency of capturing hood and penetration rate of dust separator. In addition, outdoor air volume $\mathrm{V}_{\mathrm{N}}$ is supplied into and equal air volume $\mathrm{V}_{\mathrm{L}}$ is exhausted from workshop, their respective dust concentration are $C_{N}$ and $C_{L}$, the volume of workshop is $\mathrm{V}_{\mathrm{R}}$.


Figure 1 Constant recirculate air volume ventilation and dust removing system.
According to the mass balance equation of dust, the variation rate of indoor dust concentration $C_{R}$ by time $t$ is :

$$
\begin{equation*}
\mathrm{V}_{\mathrm{R}} \frac{\mathrm{dC}_{\mathrm{R}}}{\mathrm{dt}}=\varepsilon\left(1-\eta_{\mathrm{A}}\right)+\mathrm{V}_{\mathrm{P}} \mathrm{C}_{\mathrm{P}}+\mathrm{V}_{\mathrm{N}} \mathrm{C}_{\mathrm{N}}-\mathrm{V}_{\mathrm{L}} \mathrm{C}_{\mathrm{L}}-\mathrm{V}_{\mathrm{A}} \mathrm{C}_{\mathrm{R}} \tag{mg/s}
\end{equation*}
$$

If outdoor air concentration is negligible, the dust contaminant is from two parts: one part is escaping rate of dust $\varepsilon\left(1-\eta_{A}\right)$ from capturing hood, the other is the dust rate $C_{P} V_{P}$ from recirculate air $\mathrm{V}_{\mathrm{P}}$. The dust concentration of recirculate air depends on the penetration rate E of
dust separator.

$$
\begin{equation*}
V_{P} C_{P}=\varepsilon \eta_{A} E+V_{A} C_{R} E \tag{2}
\end{equation*}
$$

If it is assumed that indoor dust contaminant can be perfect diffused immediately, the exhaust dust contaminant is also from two parts: one part is the dust rate in exhaust air $\mathrm{V}_{\mathrm{L}} \mathrm{C}_{\mathrm{L}}=\mathrm{V}_{\mathrm{L}} \mathrm{C}_{\mathrm{R}}$, the other is collection rate $\mathrm{V}_{\mathrm{A}} \mathrm{C}_{\mathrm{R}}$ by capturing hood.

Then from eq.(1), the following equation can be obtained:

$$
\begin{equation*}
\mathrm{V}_{\mathrm{R}} \frac{\mathrm{~d} \mathrm{C}_{\mathrm{R}}}{\mathrm{dt}}=\varepsilon\left(1-\eta_{\mathrm{A}}\right)+\varepsilon \eta_{\mathrm{A}} E+\mathrm{V}_{\mathrm{A}} \mathrm{C}_{\mathrm{R}} \mathrm{E}-\mathrm{V}_{\mathrm{L}} \mathrm{C}_{\mathrm{R}}-\mathrm{V}_{\mathrm{A}} \mathrm{C}_{\mathrm{R}} \tag{3}
\end{equation*}
$$

eq.(3) can be changed into:

$$
\begin{equation*}
\frac{d C_{R}}{d t}+\frac{V_{A}(1-E)+V_{I}}{V_{R}} C_{R}=\frac{\varepsilon\left[1-\eta_{A}(1-E)\right]}{V_{R}} \tag{4}
\end{equation*}
$$

where: $\lambda_{1}=\frac{\mathrm{V}_{\mathrm{A}}(1-\mathrm{E})+\mathrm{V}_{\mathrm{L}}}{\mathrm{V}_{\mathrm{R}}}$---theoretical air change rate $[1 / \mathrm{h}]$

$$
\begin{equation*}
\mathrm{A}_{1}=\frac{\varepsilon\left[1-\eta_{\mathrm{A}}(\mathrm{I}-\mathrm{E})\right]}{\mathrm{V}_{\mathrm{R}}} \tag{5}
\end{equation*}
$$

combining eq.(5), (6) and (4). We can get:

$$
\begin{equation*}
\frac{\mathrm{dC}_{\mathrm{R}}}{\mathrm{dt}}+\lambda_{1} \mathrm{C}_{\mathrm{R}}=\mathrm{A}_{1} \tag{7}
\end{equation*}
$$

It is assumed that the emission rate of dust is constant ( $\mathrm{d} \varepsilon / \mathrm{dt}=0$ ) and the initial dust concentration is negligible, eq.(7) can be solved:

$$
\begin{equation*}
C_{R}=\frac{\varepsilon\left[1-\eta_{A}(1-E)\right]}{V_{A}(1-E)+V_{L}}\left(1-e^{-\lambda_{1}}\right) \tag{8}
\end{equation*}
$$

In equilibrium condition, after enough long time, the exponential function $e^{-\lambda i t}$ tends to be zero. In most of practical ventilation systems, $\lambda_{1}$ is $2 \sim 5[1 / \mathrm{h}]$, thus 2 hours later $\mathrm{e}^{-\lambda \mathrm{lt}}$ is negligible, then the dust concentration can be expressed exactly by the following equation:

$$
\begin{equation*}
C_{R}=\frac{\varepsilon\left[1-\eta_{A}(1-E)\right]}{V_{A}(1-E)+V_{L}} \tag{9}
\end{equation*}
$$

## VARIABLE RECIRCULATE AIR VOLUME VENTLLATION AND DUST REMOVING SYSTEM

With regard to the workshop whose dust emission rate is varied greatly, the dust concentration $C_{P}$ in recirculate air fluctuates along with the dust concentration $C_{A}$. in order to control the dust concentration and save energy, when $\mathrm{C}_{\mathrm{P}}$ increases, the exhausted air volume $\mathrm{V}_{\mathrm{L}}$ and outdoor air volume $\mathrm{V}_{\mathrm{N}}$ need to be increased. This kind of system is shown in Fig.2.


Figure 2 variable recirculate air volume ventilation and dust removing system.

Referring to Fig.2, the variation rate of indoor dust concentration by time is:

$$
\begin{equation*}
\mathrm{V}_{\mathrm{R}} \frac{\mathrm{dC}_{\mathrm{R}}}{\mathrm{dt}}=\varepsilon\left(1-\eta_{\mathrm{A}}\right)+\mathrm{V}_{\mathrm{P}} \mathrm{C}_{\mathrm{P}}+\mathrm{V}_{\mathrm{N}} \mathrm{C}_{\mathrm{N}}-\mathrm{V}_{\mathrm{A}} \mathrm{C}_{\mathrm{R}} \tag{10}
\end{equation*}
$$

eq.(10) can also be changed into:

$$
\begin{equation*}
\frac{d C_{R}}{d t}+\frac{V_{A}(1-E)+V_{L} E}{V_{R}} C_{R}=\frac{\varepsilon\left\{1-\eta_{A}\left[1-E\left(1-V_{1} / V_{A}\right)\right]\right\}}{V_{R}} \tag{11}
\end{equation*}
$$

If time $t$ is greater than 2 hours, the approximate solution to eq.(11) is:

$$
\begin{equation*}
\mathrm{C}_{\mathrm{R}}=\frac{\varepsilon\left\{1-\eta_{\mathrm{A}}\left[1-\mathrm{E}\left(1-\mathrm{V}_{\mathrm{L}} / \mathrm{V}_{\mathrm{A}}\right)\right]\right\}}{\mathrm{V}_{\mathrm{A}}(1-\mathrm{E})+\mathrm{V}_{\mathrm{L}} \mathrm{E}} \tag{12}
\end{equation*}
$$

[ $\mathrm{mg} / \mathrm{m}^{3}$ ].
From eq.(12), we can concluded that when $V_{A}$ is constant, increasing the exhausted air volume $\mathrm{V}_{\mathrm{L}}$ can lead to the decrease of the indoor dust concentration $\mathrm{C}_{\mathrm{R}}$ and then prevent it from exceeding the dust concentration standard. If we can adjust the recirculate air volume $V_{P}$ and the exhausted air volume $\mathrm{V}_{\mathrm{L}}$, the indoor dust concentration can be controlled effectively.

## THE ALLOWABLE DUST CONCENTRATION $C_{P}$ IN RECIRCULATE AIR

In variable recirculate air volume ventilation system, it is assumed that the dust concentration $\mathrm{C}_{\mathrm{N}}$ in the outdoor air is zero. Eq.(10) can be changed into:

$$
\begin{equation*}
\mathrm{V}_{\mathrm{R}} \frac{\mathrm{~d} \mathrm{C}_{\mathrm{R}}}{\mathrm{dt}}=\varepsilon\left(1-\eta_{\mathrm{A}}\right)+\mathrm{V}_{\mathrm{P}} \mathrm{C}_{\mathrm{P}}-\mathrm{V}_{\mathrm{A}} \mathrm{C}_{\mathrm{R}} \tag{13}
\end{equation*}
$$

eq.(13) can also be changed into:

$$
\begin{equation*}
\frac{d C_{R}}{d t}+\frac{V_{A}}{V_{R}} C_{R}=\frac{\varepsilon\left(1-\eta_{A}\right)+V_{P} C_{P}}{V_{R}} \tag{14}
\end{equation*}
$$

If time $t$ is greater than 2 hours, the approximate solution to eq.(14) is:

$$
\begin{equation*}
\mathrm{C}_{\mathrm{R}}=\frac{\varepsilon\left(1-\eta_{A}\right)+\mathrm{V}_{\mathrm{P}} \mathrm{C}_{\mathrm{P}}}{\mathrm{~V}_{\mathrm{R}}} \tag{15}
\end{equation*}
$$

The dust concentration in recirculate air is that in air out of dust separator, it depend on the total air volume $\mathrm{V}_{\mathrm{A}}$, the dust emission rate $\varepsilon$, the collection efficiency $\eta_{\mathrm{A}}$ of capturing hood and the penetration rate $E$ of dust separator:

$$
\begin{gather*}
\mathrm{C}_{\mathrm{P}}=\mathrm{C}_{\mathrm{A}} \mathrm{E}=\left(\frac{\varepsilon \eta_{\mathrm{A}}}{\mathrm{~V}_{\mathrm{A}}}+\mathrm{C}_{\mathrm{R}}\right) \mathrm{E} \\
\varepsilon\left(1-\eta_{\mathrm{A}}\right)=\frac{\mathrm{V}_{\mathrm{A}}\left(1-\eta_{\mathrm{A}}\right)}{\eta_{\mathrm{A}}}\left(\frac{\mathrm{C}_{\mathrm{P}}}{\mathrm{E}}-\mathrm{C}_{\mathrm{R}}\right) \tag{16}
\end{gather*}
$$

combing eq.(15) and (16):

$$
\begin{equation*}
\mathrm{C}_{\mathrm{R}}=\frac{1-\eta_{\mathrm{A}}+\frac{\mathrm{V}_{\mathrm{P}}}{\mathrm{~V}_{\mathrm{A}}} \eta_{\mathrm{A}} \mathrm{E}}{\mathrm{E}} \mathrm{C}_{\mathrm{P}} \tag{17}
\end{equation*}
$$

This expression shows the relation between the dust concentration $C_{P}$ in recirculate air and the indoor dust concentration $\mathrm{C}_{\mathrm{R}}$. It is assumed that air leakage of the whole system is negligible and the exhausted air volume $\mathrm{V}_{\mathrm{C}}$ is equal to $20 \% \mathrm{~V}_{\mathrm{A}}$, so the recirculate air volume $\mathrm{V}_{\mathrm{P}}$ is equal to $80 \% \mathrm{~V}_{\mathrm{A}}$. If collection efficiency of capturing hood $\eta_{\mathrm{A}}$ and the penetration rate E of dust separator are supposed to be 0.98 and 0.01 respectively, from the eq.(17) we can obtain:

$$
\mathrm{C}_{\mathrm{R}}=2.78 \mathrm{C}_{\mathrm{P}}
$$

because $C_{R}$ should be lower than maximum allowable concentration $C_{\text {Max }}$, then:

$$
\mathrm{C}_{\mathrm{P}}<0.36 \mathrm{C}_{\mathrm{MAX}} \cong 1 / 3 \mathrm{C}_{\mathrm{MAX}}
$$

Based on the above value of $\mathrm{V}_{\mathrm{L}}, \mathrm{V}_{\mathrm{P}}, \eta_{\mathrm{A}}$ and E , we can concluded that dust concentration $\mathrm{C}_{\mathrm{P}}$ should be lower than $1 / 3$ of the maximum allowable concentration $C_{\text {max }}$ and $80 \%$ of the total consumed energy can be saved with perfect thermal insulation of the system.

THE RELATTVE EUUMIDITY OF RECIRCULATE AIR VENTILATION SYSTEM
In the workshop with high moisture gain, the indoor air humidity ratio gradually increase due to the use of recirculate air ventilation system. So in order to maintain the indoor relative humidity within the range of acceptable standards for occupational health and production requirement. For two system mentioned above, The moisture flowchart is shown in Fig.3.


Figure 3 Moisture flowchart
Referring to Fig.3, it is supposed that the moisture gain $G$ is well distributed and the ventilation system is perfect insulated without dew and air leakage, the humidity ratio of recirculate air is equal to that of indoor air and total air volume $V_{A}$ is equal to the sum of recirculate air volume $V_{p}$ and exhausted air volume $V_{L}$. If outdoor air volume $V_{B}$ is equal to $V_{L}$ and outdoor air humidity ratio defined as $d_{N}$, the variation rate of indoor air humidity ratio by time $t$ is:

$$
\begin{equation*}
\mathrm{V}_{\mathrm{R}} \gamma_{2} \frac{\mathrm{~d}\left(\mathrm{~d}_{\mathrm{R}}\right)}{\mathrm{dt}}=\mathrm{G}+\mathrm{V}_{\mathrm{P}} \gamma_{2} \mathrm{~d}_{\mathrm{P}}+\mathrm{V}_{\mathrm{N}} \gamma_{1} \mathrm{~d}_{\mathrm{N}}-\mathrm{V}_{\mathrm{A}} \gamma_{2} \mathrm{~d}_{\mathrm{R}} \tag{18}
\end{equation*}
$$

where: $\gamma_{1}$--ooutdoor air density $\left[\mathrm{kg} / \mathrm{m}^{3}\right]$

$$
\begin{align*}
& \gamma_{2} \text {---indoor air density }\left[\mathrm{kg} / \mathrm{m}^{3}\right] \\
& \qquad \mathrm{d}_{\mathrm{P}}=\mathrm{d}_{\mathrm{R}} \tag{19}
\end{align*}
$$

The eq.(19) and (20) are put into eq.(18):

$$
\begin{equation*}
\mathrm{V}_{\mathrm{R}} \gamma_{2} \frac{\mathrm{~d}\left(\mathrm{~d}_{\mathrm{R}}\right)}{\mathrm{dt}}=\mathrm{G}+\left(\mathrm{V}_{\mathrm{A}}-\mathrm{V}_{\mathrm{L}}\right) \gamma_{2} \mathrm{~d}_{\mathrm{P}}+\mathrm{V}_{\mathrm{N}} \gamma_{1} \mathrm{~d}_{\mathrm{N}}-\mathrm{V}_{\mathrm{A}} \gamma_{2} \mathrm{~d}_{\mathrm{R}} \tag{21}
\end{equation*}
$$

If the time $t$ is grater than 2 hours, the approximate solution to eq.(21) can be obtained:

$$
\begin{equation*}
\mathrm{d}_{\mathrm{R}}=\frac{\mathrm{G}+\mathrm{V}_{1} \gamma_{1} \mathrm{~d}_{\mathrm{N}}}{\gamma_{2} \mathrm{~V}_{\mathrm{L}}} \tag{22}
\end{equation*}
$$

eq.(22) can be developed into:

$$
\begin{equation*}
\mathrm{V}_{\mathrm{L}}=\frac{\mathrm{G}}{\gamma_{2} \mathrm{~d}_{\mathrm{R}}-\gamma_{1} \mathrm{~d}_{\mathrm{L}}} \tag{23}
\end{equation*}
$$

Humidity ratio expression:

$$
\begin{equation*}
\mathrm{d}=622 \frac{\mathrm{P}_{\mathrm{b}}}{\mathrm{~B}-\Phi \mathrm{P}_{\mathrm{b}}} \tag{24}
\end{equation*}
$$

where: $\Phi$----relative humidity [\%]
$\mathrm{P}_{\mathrm{b}}$---saturation water vapor partial pressure [ Pa ]
B----atmospheric pressure $[\mathrm{Pa}]$
Combing eq.(24) and (23), we can get the exhausted air volume $V_{L}$ expression needed to maintain indoor relative humidity:

$$
\begin{equation*}
\mathrm{V}_{\mathrm{L}}=\frac{\mathrm{G}\left(\mathrm{~B}-\Phi_{\mathrm{R}} \mathrm{P}_{\mathrm{bR}}\right)\left(\mathrm{B}-\Phi_{\mathrm{N}} \mathrm{P}_{\mathrm{bN}}\right)}{622\left[\Phi_{\mathrm{R}} \mathrm{P}_{\mathrm{bR}}\left(\mathrm{~B}-\Phi_{\mathrm{N}} \mathrm{P}_{\mathrm{bN}}\right) \gamma_{2}-\Phi_{\mathrm{N}} \mathrm{P}_{\mathrm{bN}}\left(\mathrm{~B}-\Phi_{\mathrm{R}} \mathrm{P}_{\mathrm{bR}}\right) \gamma_{1}\right]} \tag{25}
\end{equation*}
$$

where: $\Phi_{\mathrm{R}}$---relative humidity of indoor air [\%]
$\Phi_{\mathrm{N}}--$-relative humidity of outdoor air [\%]
$\mathrm{P}_{\mathrm{bR}}---$-saturation water vapor partial pressure of indoor air $[\mathrm{Pa}]$
$\mathrm{P}_{\mathrm{bN}--- \text {-saturation water vapor partial pressure of outdoor air }[\mathrm{Pa}]}$
If most of the air harmful \& contaminants in workshop is moisture, we can adjust exhaust air value and control the relative humidity of indoor air. The function relation between humidity and exhaust air volume $V_{L}$ can be expressed as:

$$
\begin{equation*}
\Phi_{R}=\frac{\left(\mathrm{G}+\mathrm{d}_{\mathrm{N}} \mathrm{~V}_{\mathrm{L}} \gamma_{1}\right) \mathrm{B}}{\left(622 \mathrm{~V}_{\mathrm{L}} \gamma_{2}+\mathrm{G}+\mathrm{d}_{\mathrm{N}} \mathrm{~V}_{\mathrm{L}} \gamma_{1}\right) \mathrm{P}_{\mathrm{bR}}} \tag{26}
\end{equation*}
$$

## THE CALCULATION OF HEATER CAPACITY

The calculation and selection of heater capacity in this system depend on the condition of service. For the workshop of intermittent service, heating must be rapid. The calculation of heater should depend on the time during which the workshop is heated required by users. According to the conservation theory of energy:

$$
\begin{align*}
C \frac{d \theta}{d t} & =\gamma+G_{E} C^{\prime} \theta_{0}-Q^{\prime}-G_{E} C^{\prime} \theta \\
& =\gamma q+G_{E} C^{\prime} \theta_{0}-\frac{\theta-\theta^{\prime}}{R} m-G_{E} C^{\prime} \theta \tag{27}
\end{align*}
$$

where: C-rratio of specific heats (include the heat accumulated by equipment) $\left[\mathrm{kw} /{ }^{\circ} \mathrm{C}\right]$
$\theta$----indoor air temperature [ $\left.{ }^{\circ} \mathrm{C}\right]$
$\gamma$---vaporization latent heat [kw/kg]
q----flow rate of water vapor into heater [ $\mathrm{kg} / \mathrm{h}$ ]
$\mathrm{G}_{\mathrm{E}}$--supply air, return air volume [kg/h]
C'----specific heat of air [kw/kg. $\left.{ }^{\circ} \mathrm{C}\right]$
$\theta_{0}---$-temperature of supply air before heater [ ${ }^{\circ} \mathrm{C}$ ]
Q'---heat transfer rate through the explosure of workshop [kw/h]
$\theta^{\prime}$---outer wall temperature of explosure [ $\left.{ }^{\circ} \mathrm{C}\right]$
R ---heat resistance of explosure [ $\mathrm{m}^{2} \cdot \mathrm{~h} \cdot{ }^{\circ} \mathrm{C} / \mathrm{kw}$ ]
m --area of the explosure $\left[\mathrm{m}^{2}\right]$
Eq.(27) can be developed into:

$$
\begin{equation*}
\frac{\mathrm{RC}}{\mathrm{~m}+\mathrm{RG}_{\mathrm{E}} \mathrm{C}^{\prime}} \frac{\mathrm{d} \theta}{\mathrm{dt}}+\theta=\frac{\mathrm{RG}_{\mathrm{E}} \mathrm{C}^{\prime}}{\mathrm{m}+\mathrm{RG}_{\mathrm{E}} \mathrm{C}^{\prime}}\left(\frac{\gamma q}{\mathrm{G}_{\mathrm{E}} \mathrm{C}^{\prime}}+\theta_{0}+\frac{\mathrm{m}}{\mathrm{RG}_{\mathrm{E}} \mathrm{C}^{\prime}} \theta^{\prime}\right) \tag{28}
\end{equation*}
$$

where we define: $T=\frac{R C}{m+R G_{E} C^{\prime}} \quad---$-time constant of the control object

$$
\begin{aligned}
& \mathrm{K}=\frac{\mathrm{RG}_{\mathrm{E}} \mathrm{C}^{\prime}}{\mathrm{m}+\mathrm{RG}_{\mathrm{E}} \mathrm{C}^{\prime}} \quad--- \text { coefficient of amplification } \\
& \theta_{r}=\frac{\gamma q^{\mathrm{G}_{\mathrm{E}} \mathrm{C}^{\prime}}+\theta_{0}+\frac{\mathrm{m}}{\mathrm{RG}_{\mathrm{E}} \mathrm{C}^{\prime}} \theta \quad-- \text { input }}{} .
\end{aligned}
$$

Then eq.(28) can be expressed as:

$$
\begin{equation*}
\mathrm{T} \frac{\mathrm{~d} \theta}{\mathrm{dt}}+\Delta \theta=\mathrm{K} . \mathrm{\lambda} \theta_{y} \tag{29}
\end{equation*}
$$

If $t=t_{0}=0, \Delta \theta_{0}=0, \Delta \theta^{\prime}=0$, then $\Delta \theta_{r}=\gamma q / G_{\varepsilon} C^{\prime}$. When the heating system starts, the flow rate of water vapor into heater is $q$, whose amplitude as a transition heat rate is defined as $M=\Delta \theta_{r}$. The solution to eq.(29) is:

$$
\begin{equation*}
\Delta \theta=K M\left(1-e^{-1 / T}\right) \tag{30}
\end{equation*}
$$

As expressed by eq.(30), the relation between temperature increment $\Delta \theta$ and time $t$ can be described as exponential curve. The calculation cyuation of heater capacity can be obtained by eq.(30) with $M=\gamma q / G_{E} C^{\prime}$ :

$$
\begin{equation*}
Q=\frac{G_{ \pm}(C \Delta \theta}{K\left(1-e^{-3 / T}\right)} \tag{kwh}
\end{equation*}
$$

where: $\Delta \theta$----the maximum increment of indoor air temperature $\left[{ }^{\circ} \mathrm{C}\right]$
The time constant and coefficient of amplitication in eq.(31) can be expressed as the following equations by using that of thermostatic room.

$$
\mathrm{K}=\frac{\mathrm{T}=90 / \mathrm{N} \quad[\mathrm{~min}]}{1+\frac{52}{\mathrm{~N}}\left(\frac{1}{\mathrm{a}}+\frac{1}{\mathrm{~b}} \cdot \frac{1}{\mathrm{~h}}\right)} \quad\left[{ }^{\circ} \mathrm{C} /{ }^{\circ} \mathrm{C}\right]
$$

where: N --air change rate
$\mathrm{a}, \mathrm{b}, \mathrm{h}$--length, width and height of wor , shop [ m ]
Referring to eq.(31), we can conclude that \$surter heating time $t$ results in higher capacity of heater. For example, if air change rate N of werishop is 5 , the constant of time is:

$$
\mathrm{T}=90 / \mathrm{N}=9 \%_{\mathrm{s}}=18 \quad[\mathrm{~min}]
$$

Apparently we can see that with the heater capasic calculated by using 3 times constant of time, it will take about 54 minutes to elevate indoor temperature to that as expected.

THE ENERGY SAVING OF RECRICUL.ATE AIR VENTILATION AND DUST CONTROL GYSTEM

In the frigid zone of northern China with hisir. remperature difference between outdoor and indoor air, while the ordinary ventilation and duss control system are running, a large quarnity of heated air is exhausted and outdoor cold air $\approx$ supplied. So considerable energy is wasteld Adopting recirculate air ventilation system can sintribute to energy save while guarantecirf indoor dust concentration below the acceptable srandard for health. So far this kind of sytue has been set up in some plants. It was estimatei that the average air flow rate of a ventilatice system is about $10000 \mathrm{~m}^{3} / \mathrm{h}$ and more than 1000 ventilation systems will be set up. It is dec assumed that the economic effect by adopting this system is $¥ 8000$ and $¥ 4700$ for frigid aff cold zone respectively.

